



Part A: Dissolved Oxygen (DO) Trends at SWIFT RC

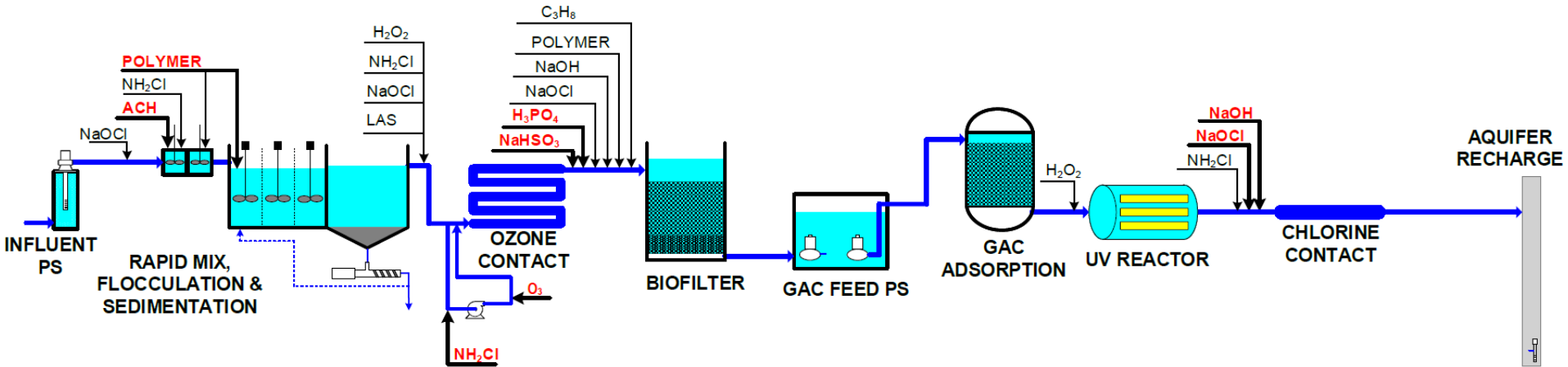
Upgrades to control of SWIFT Water DO (independent of TOC)

Part B: James River SWIFT Process Concepts

SWIFT Research Center Developments Applied to the James River SWIFT Design

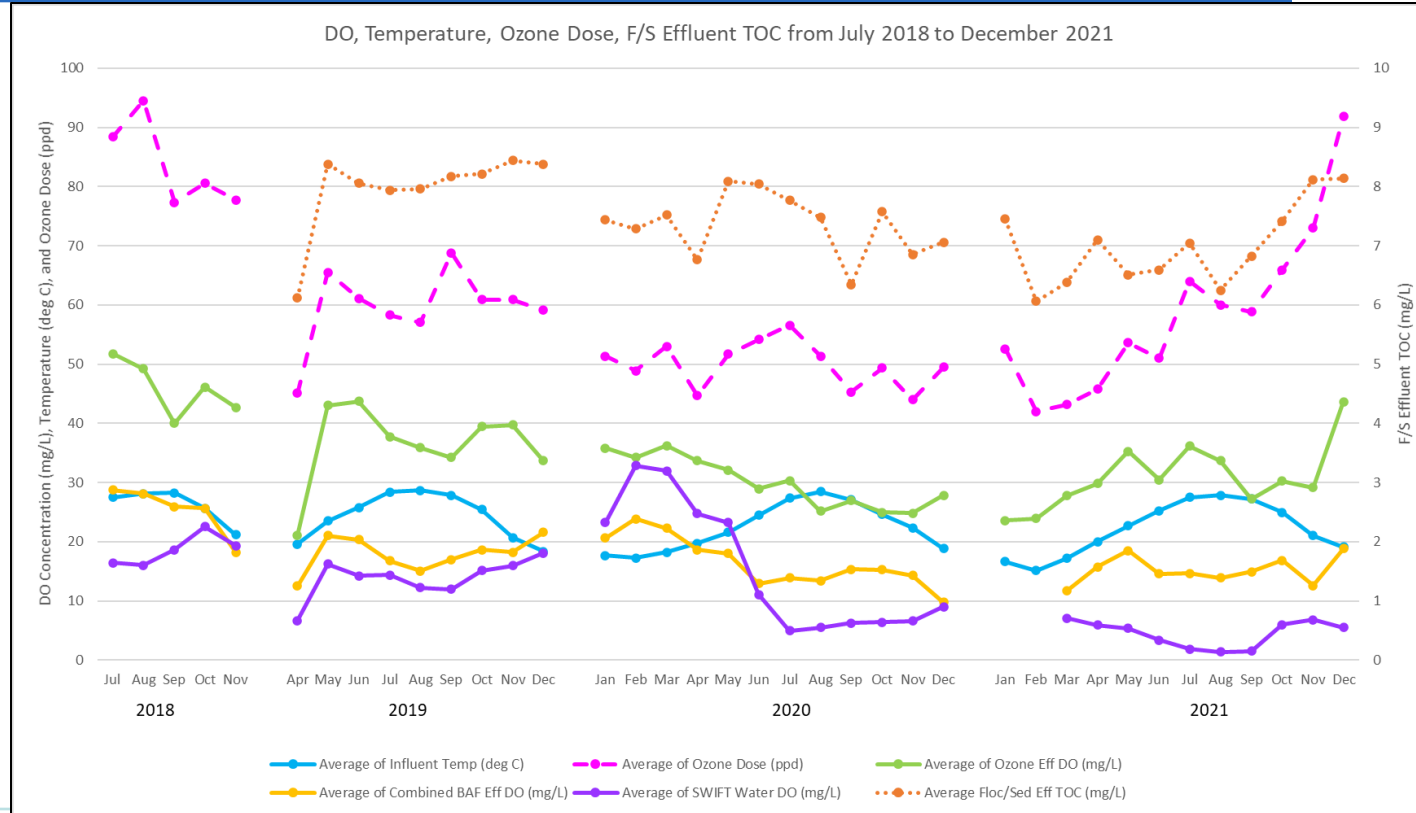


SWIFT Research Center (Current active chemicals)

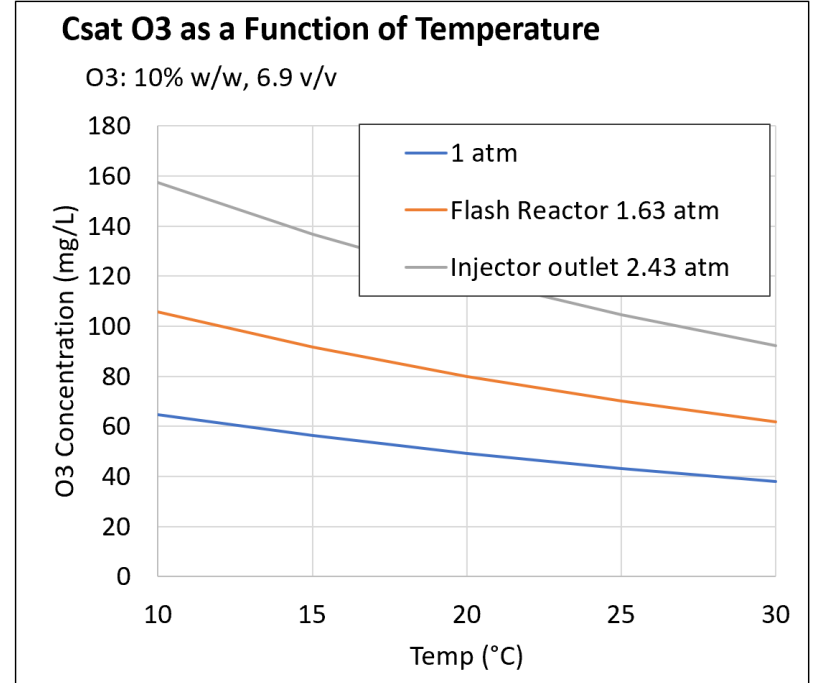
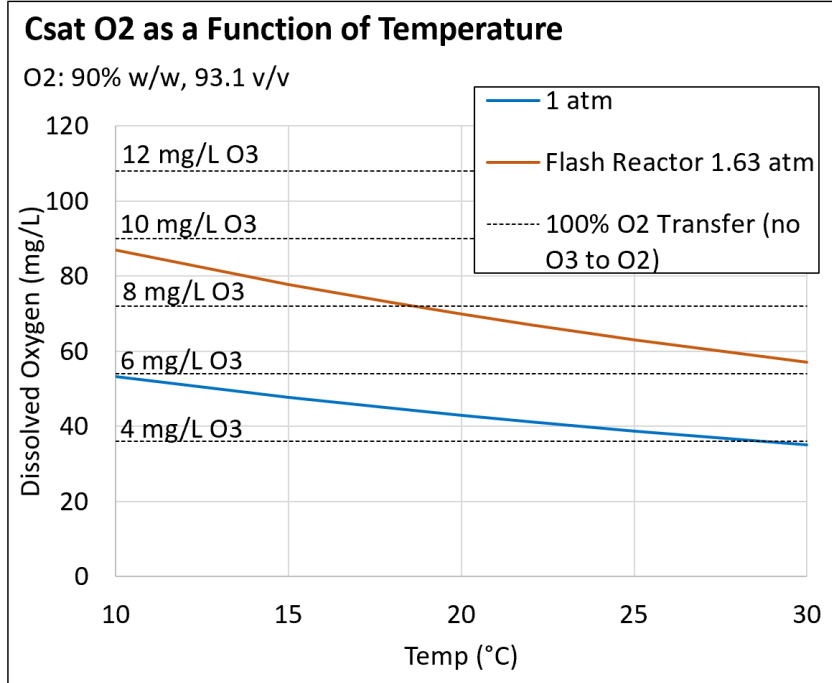


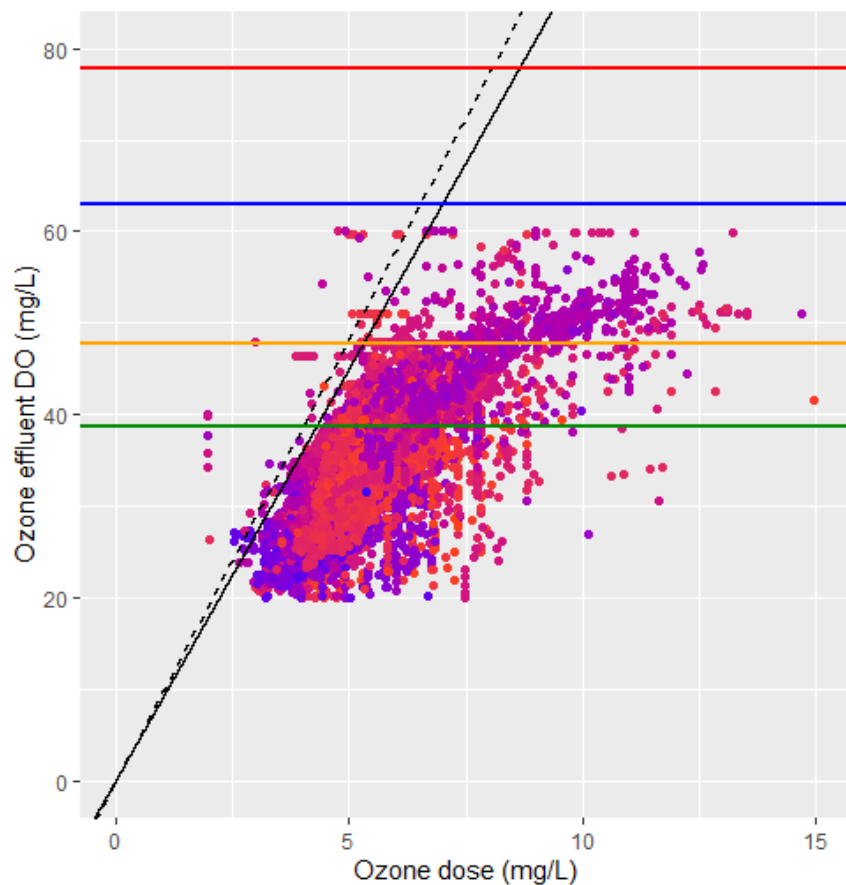
Ozone Dose and DO

- O3 dose and F/S TOC trend well together
- O3 dose and O3 effluent DO generally trend well together
- O3 dose has averaged 40-55 ppd for 2020 but increased in 2021
- SWIFT Water DO consistently 5-10 mg/L, but low in summer 2021



10% w/w Ozone = 6.9% v/v. N_2 volume negligible \rightarrow 93.1% O_2



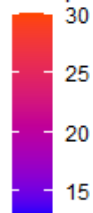


Csat O₂: 93.1 %v/v, 90 %w/w

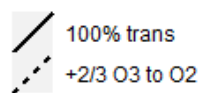
- 1.63 atm, 15° C
- 1.63 atm, 25° C
- 1 atm, 15° C
- 1 atm, 25° C

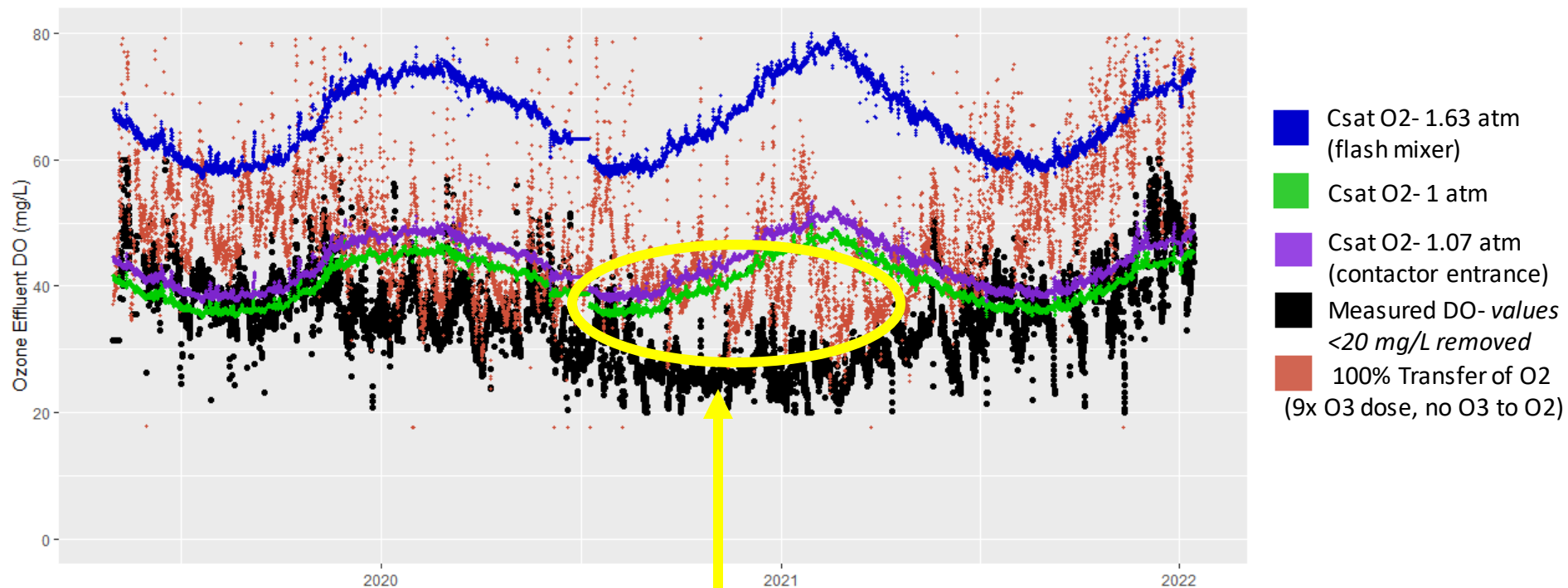
Values <20 mg/L removed

Temp

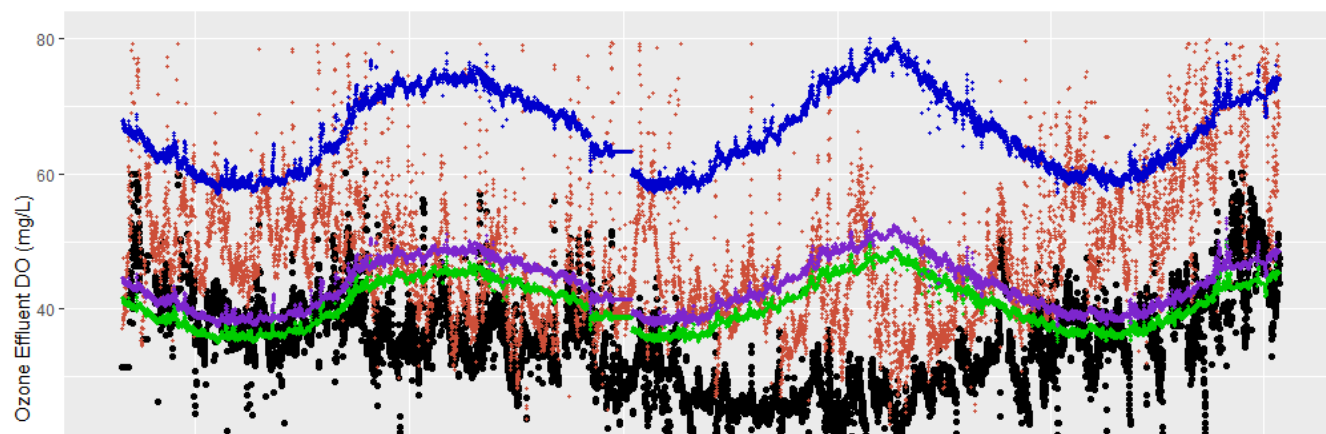


100% O₂ Transfer

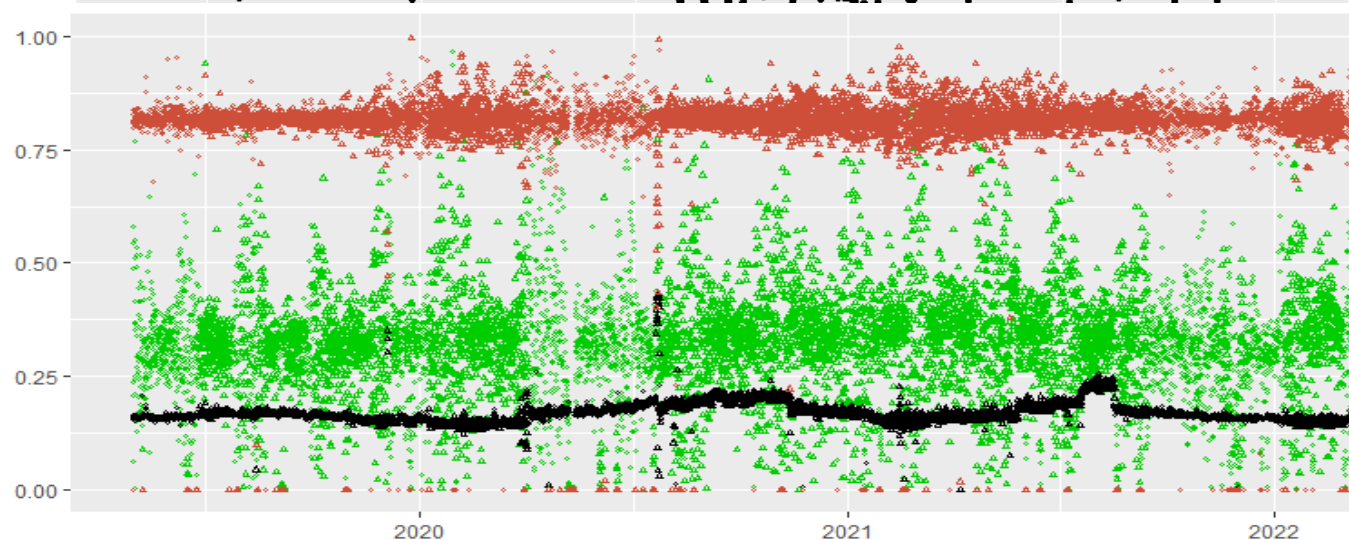




Are we dosing the ozone that we think we are?



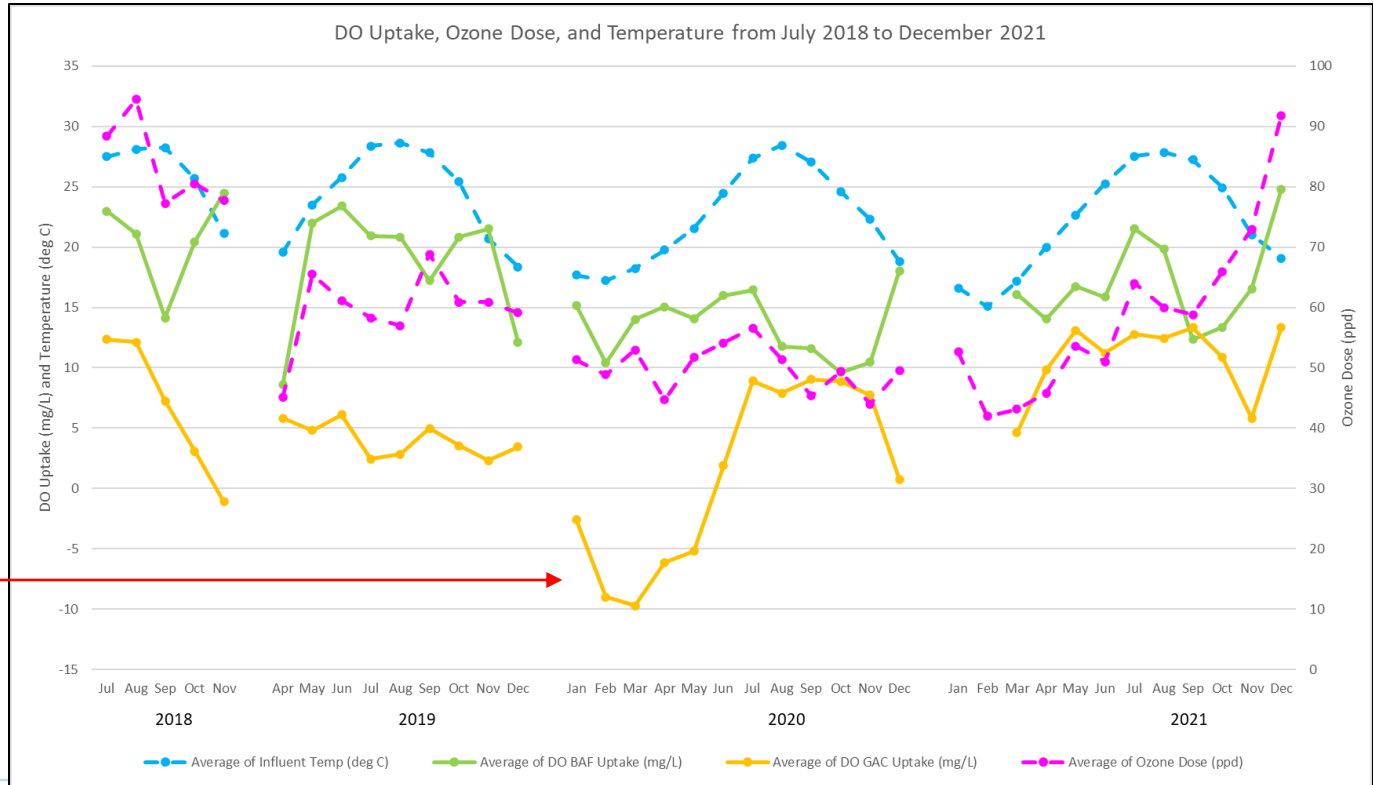
- Csat O2- 1.63 atm (flash mixer)
- Csat O2- 1 atm
- Csat O2- 1.07 atm (contactor entrance)
- Measured DO- values <20 mg/L removed
- 100% Transfer of O2 (9x O3 dose, no O3 to O2)



- Gas Flow*Conc/O3 ppd
- Lox tank level change (in/hr) /O3 ppd
- Generator efficiency kW/O3 ppd

DO Uptake Comparison

- DO uptake across BAF has consistently been 10-20 mg/L through 2020 and 2021
- Since recalibration, GAC uptake has consistently been 3-13 mg/L
- SWIFT DO probe recalibration

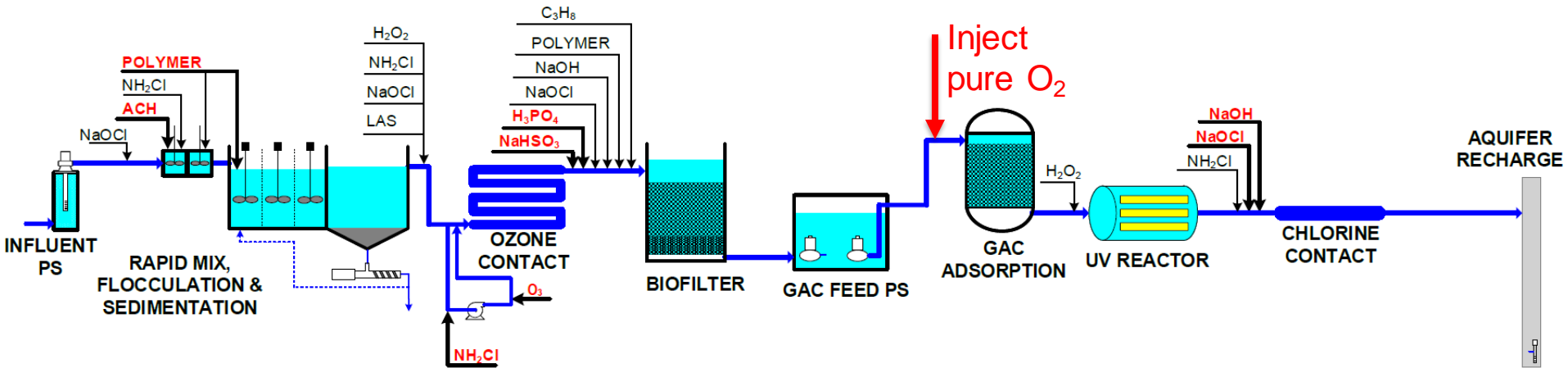


Factors Causing Low SWIFT Water DO

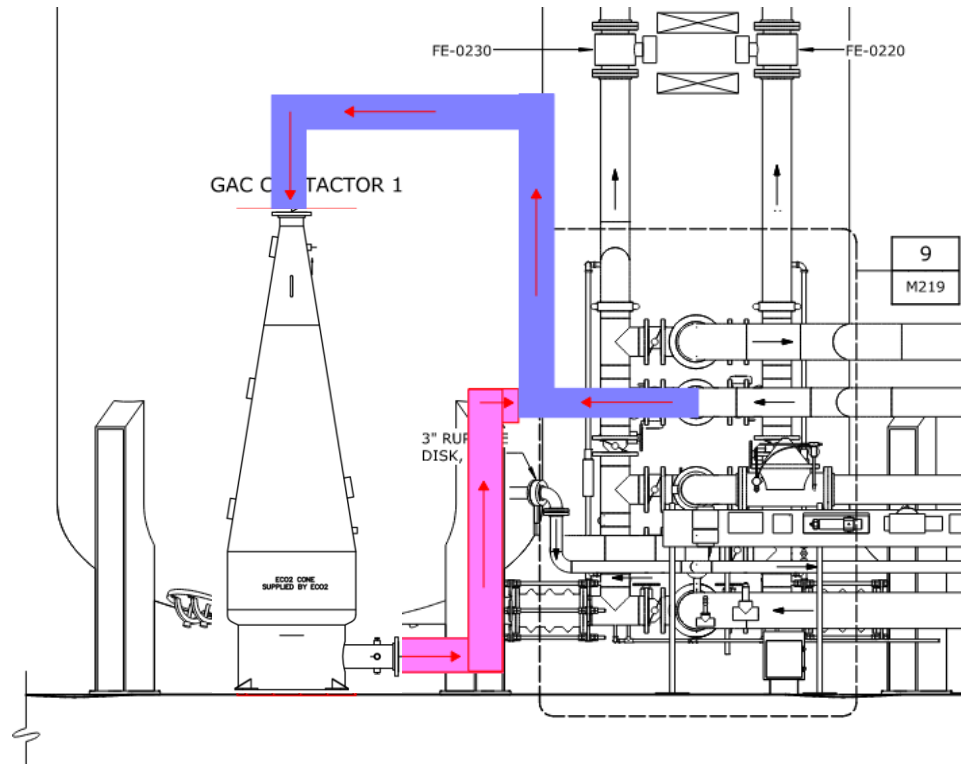
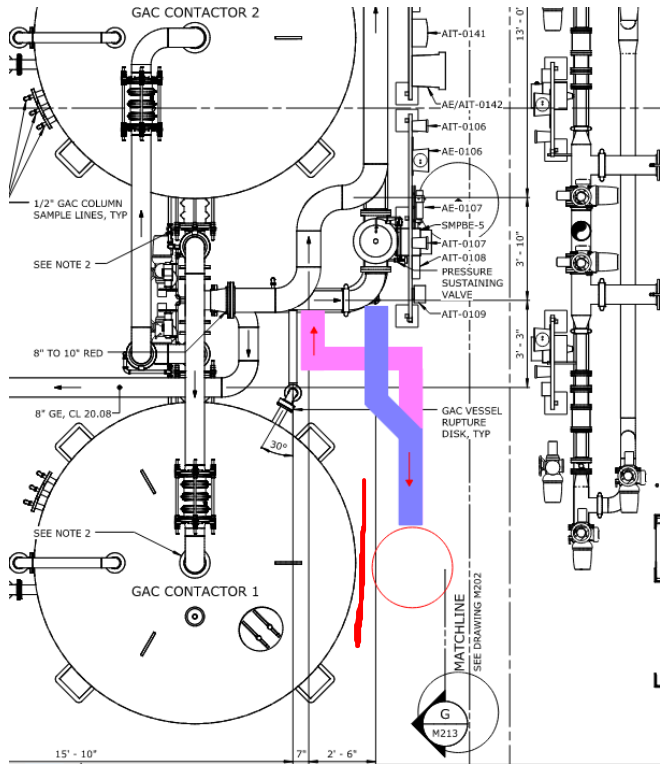
- Low O₃ Demand – Less O₂ gas flow introduced to water
- High Temperature – Lower O₂ solubility, more loss from GAC feed pump station wetwell, more biological uptake in BAF and GAC
- Low Flow – more loss from GAC feed pump station wet well, more biological uptake in BAF and GAC
- High BVs on GAC – More biological uptake of O₂
- End of 2020, inexplicably low ozone effluent DO



SWIFT Research Center (Current active chemicals)



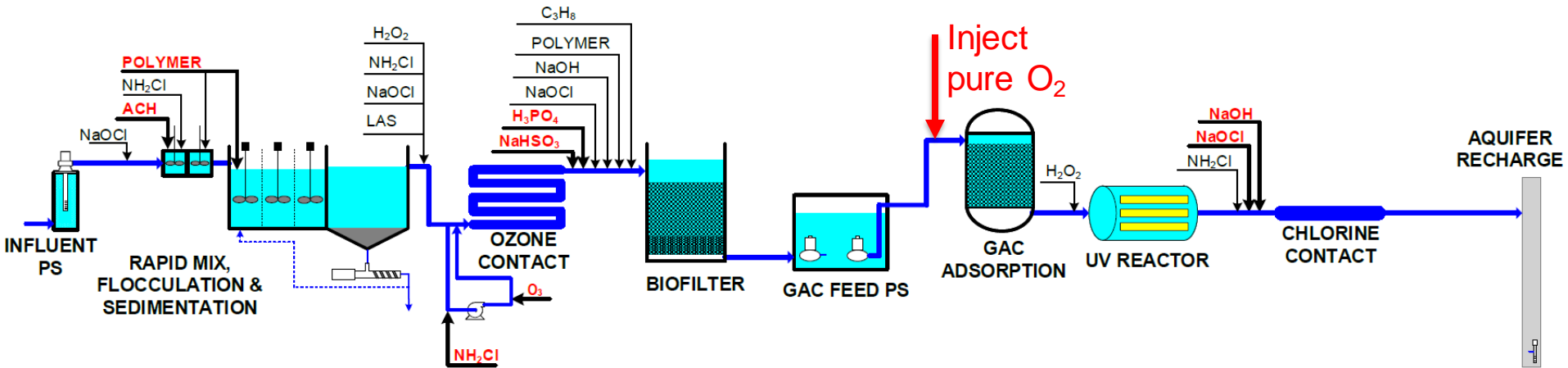
Speece Cone Design – Installed Adjacent to GAC Contactor 1



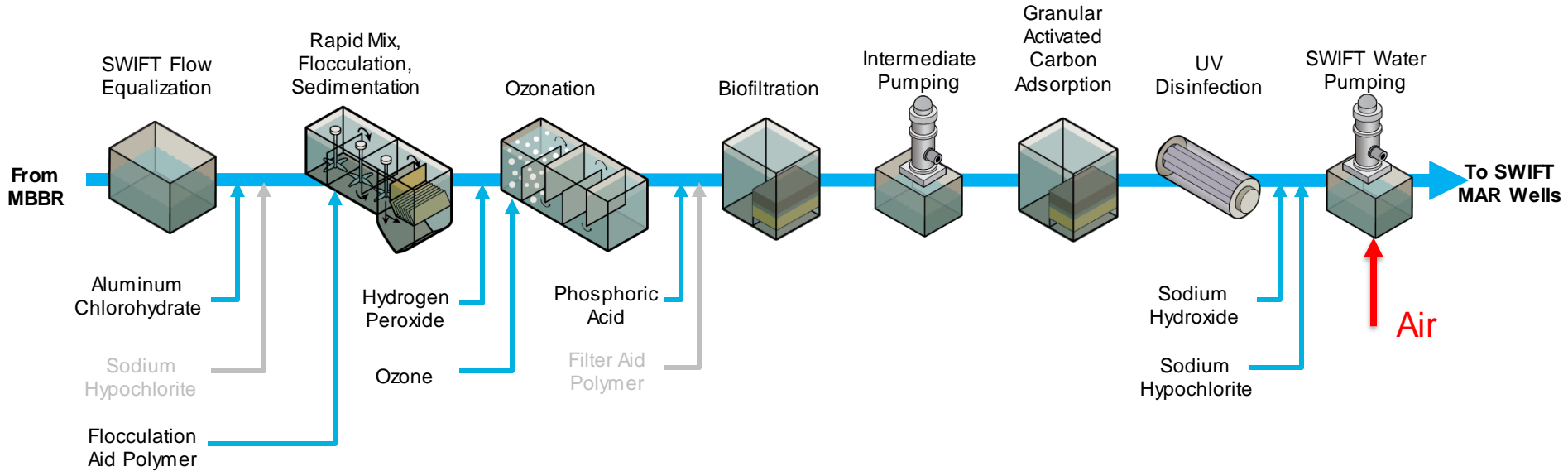
Speece Cone Example



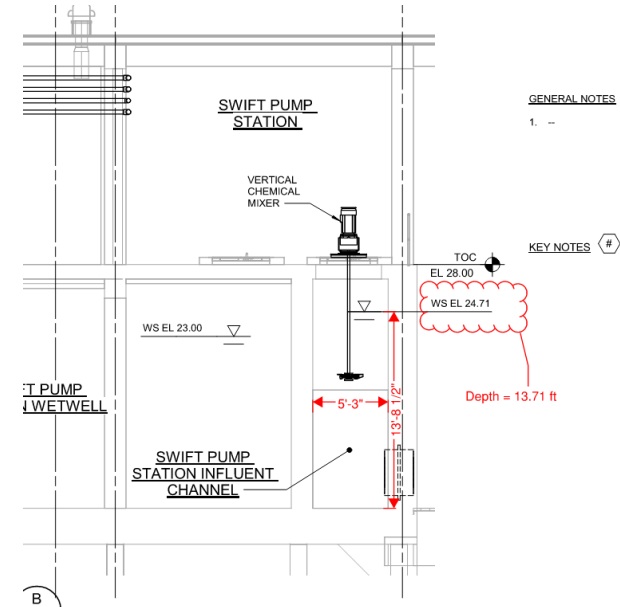
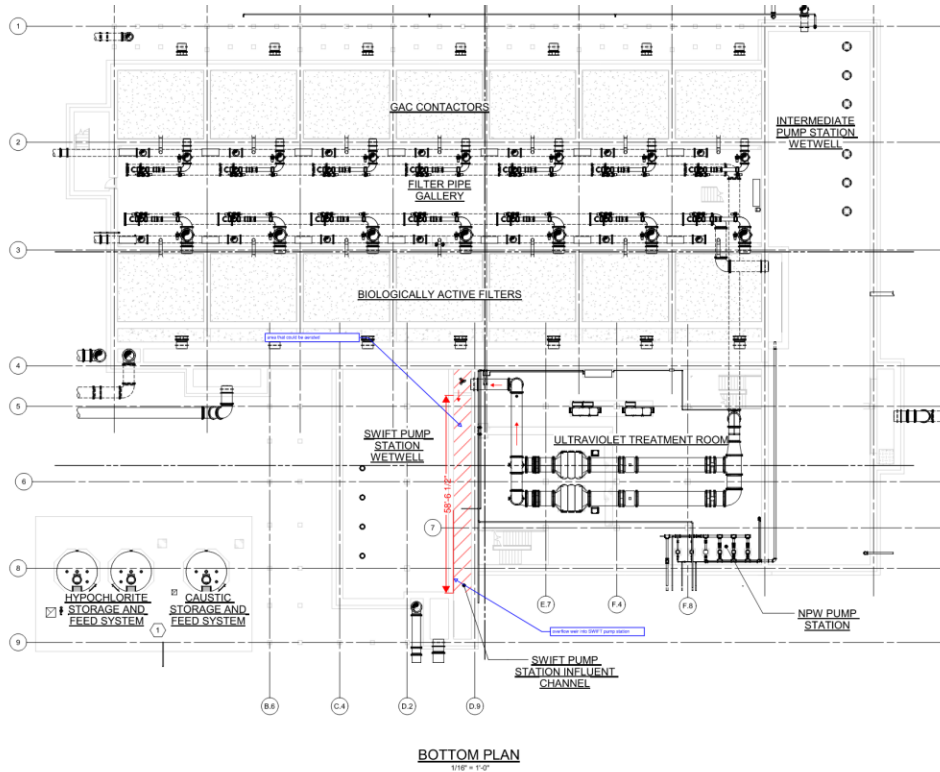
SWIFT Research Center (Current active chemicals)



James River SWIFT Process Flow Diagram



Potential Diffuser Location – SWIFT PS Wetwell Influent Channel



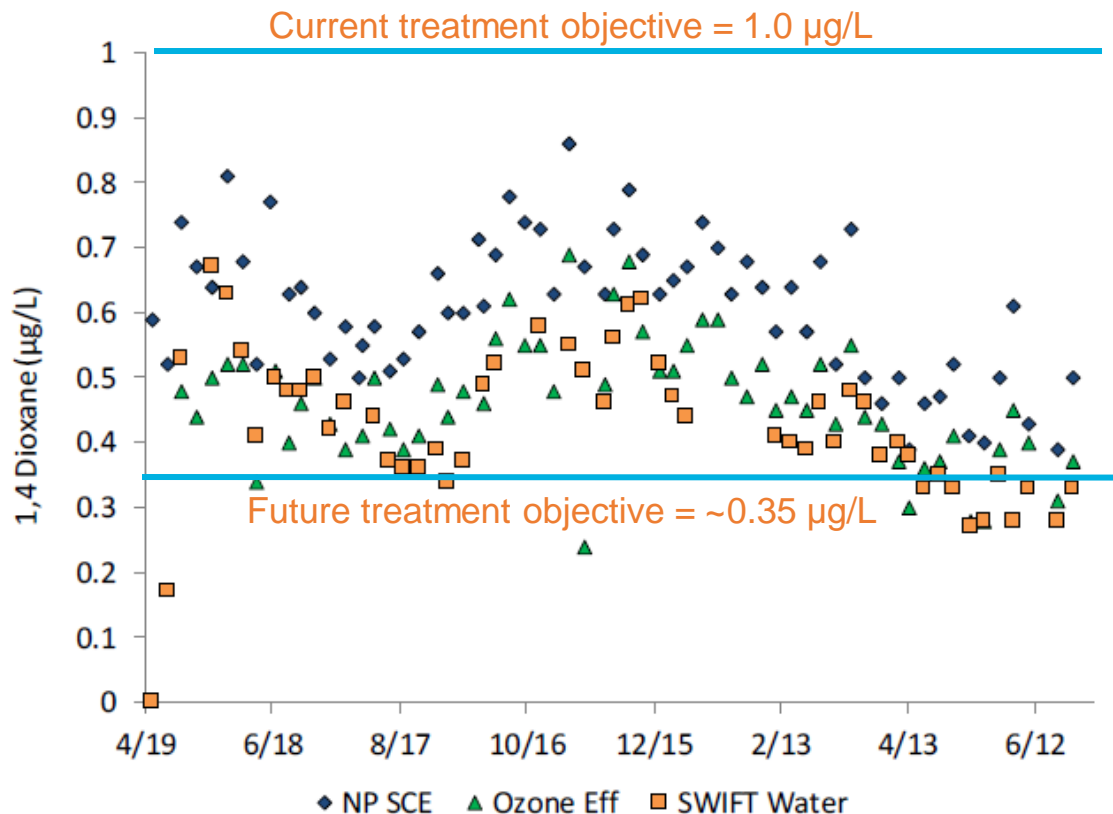
Part B: James River SWIFT Process Concepts

SWIFT Research Center Developments Applied to the James River SWIFT Design

- Improved control of 1,4-dioxane at Bethel Landfill
- Ozone with hydrogen peroxide and multi-point fine bubble dissolution
- Propane for enhanced 1,4-dioxane removal in biofilters?
- Free chlorine only for recharge well protection
- Ozone/BAF for wastewater disinfection



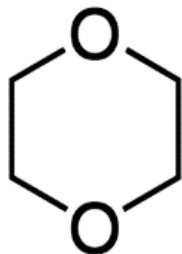
SWIFT Research Center 1,4-Dioxane



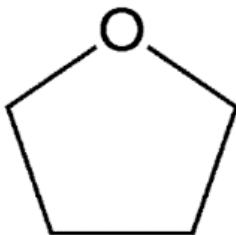
HRSD 1,4-dioxane (µg/L) Secondary Effluent

| | ABTP | BHTP | JRTP | VIPTP | WBTP | YRTP |
|---------|------|------|-------------|-------|------|------|
| Min | 0.48 | 0.55 | 0.74 | 0.49 | 0.52 | 0.34 |
| Max | 0.68 | 0.74 | 1.6 | 2.2 | 0.71 | 0.66 |
| Average | 0.56 | 0.64 | 1.12 | 0.93 | 0.61 | 0.48 |

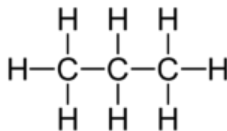
Biofilter Pilot – Co-metabolic removal of 1,4-dioxane using tetrahydrofuran or propane



1,4-Dioxane



Tetrahydrofuran
(THF)



Propane

(Cordone et al., 2016; Zenker et al., 2004)

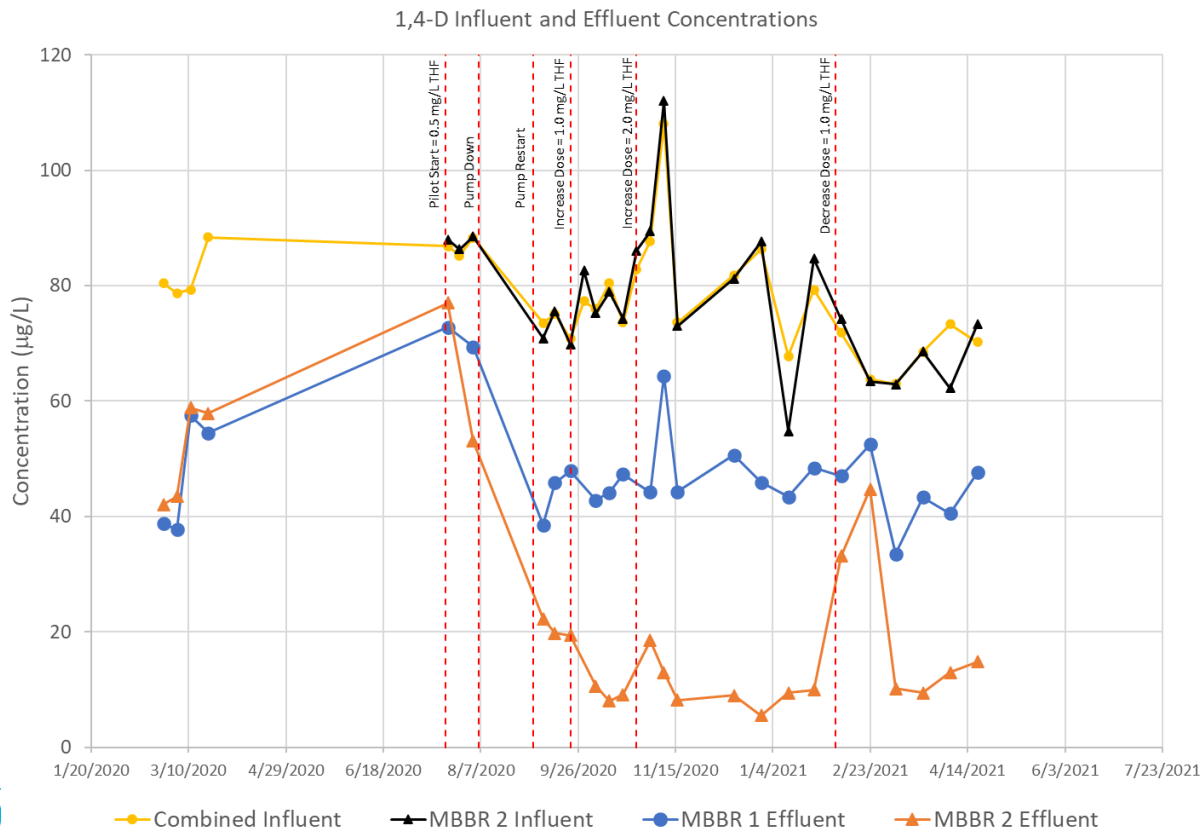
(Deng et al., 2018; Li et al., 2020; Mahendra et al., 2007)



Waste Management – Bethel Landfill Leachate Pretreatment System



THF Addition to MBBR2 Improved 1,4-Dioxane Removal



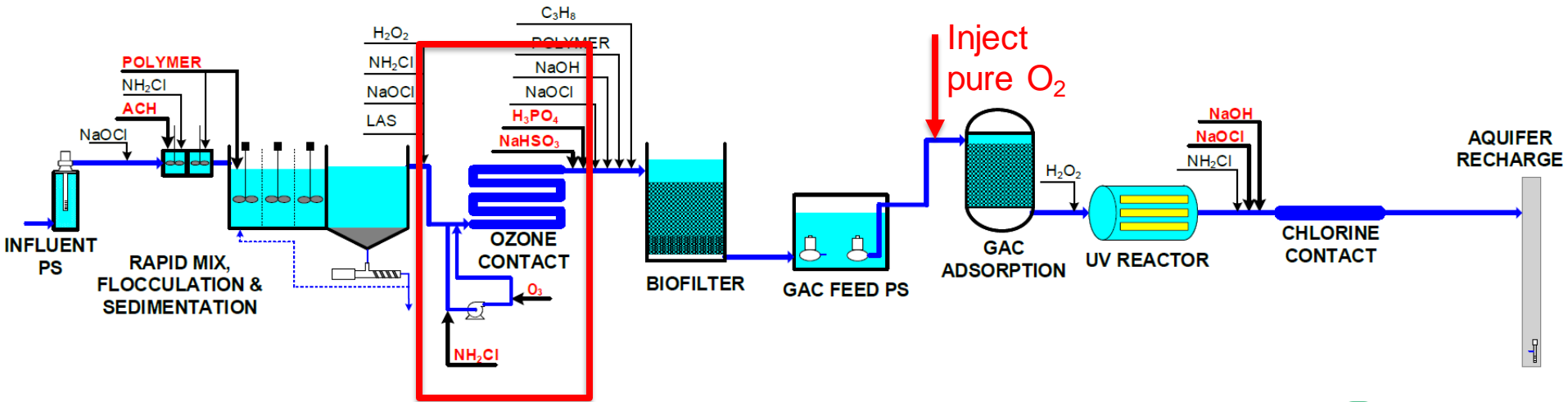
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SWIFT Research Center (Current active chemicals)



Ozonation at JR SWIFT

Liquid Oxygen Storage and Vaporizers



Hydrogen Peroxide
From Sedimentation Basins

Ozone Destruct



Oxygen Gas

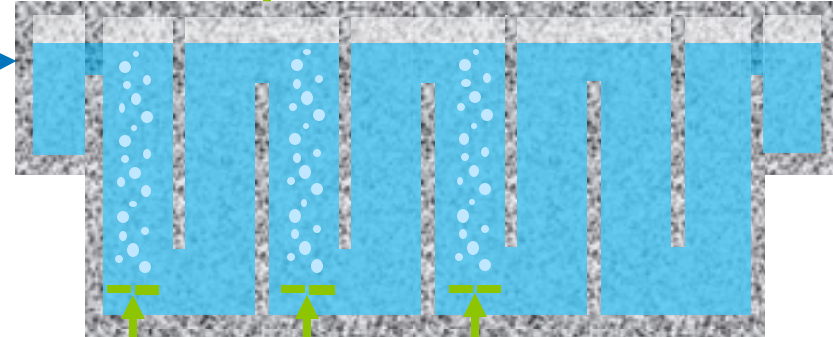
To Biofilters

Gaseous Oxygen

Ozone Gas

Ozone Generators

Nitrogen Boost

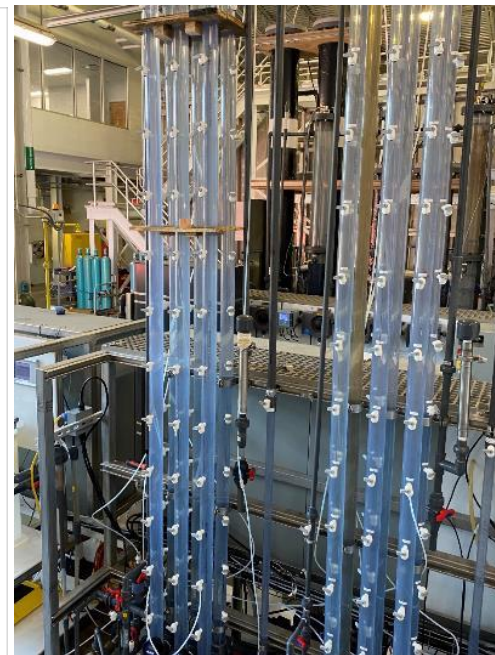
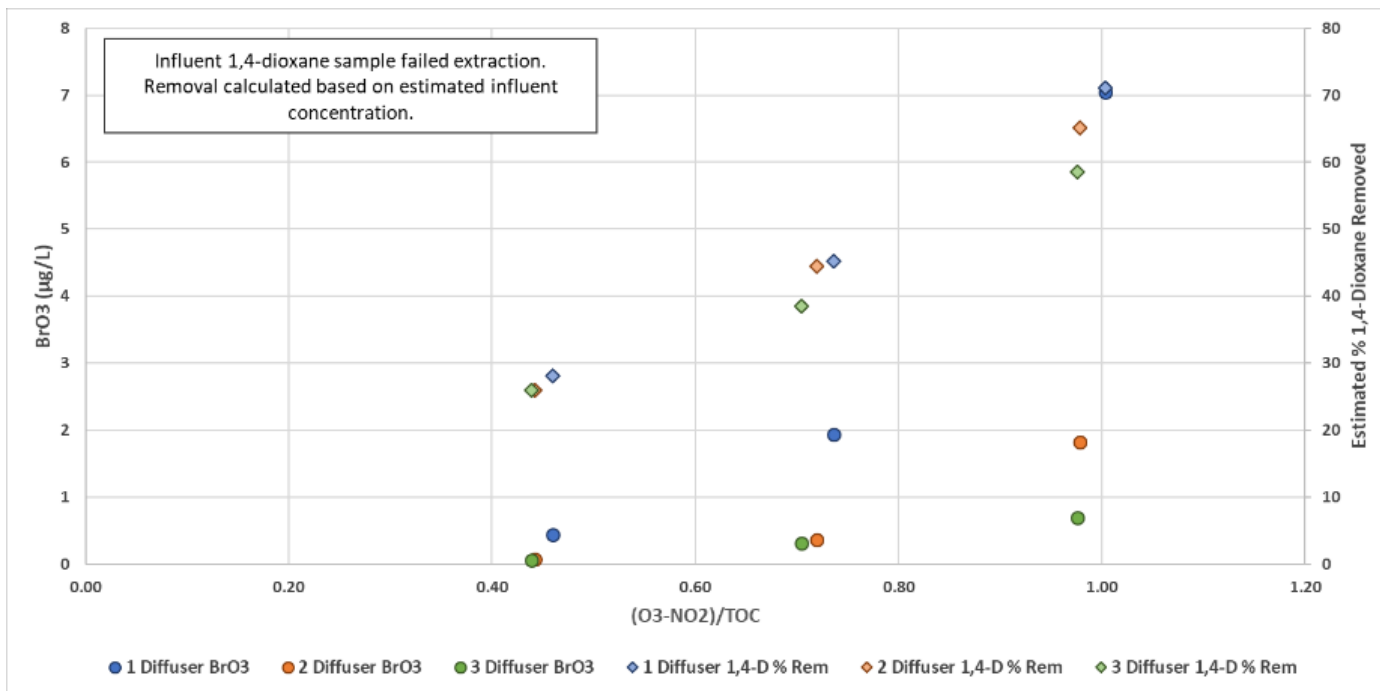


M

M

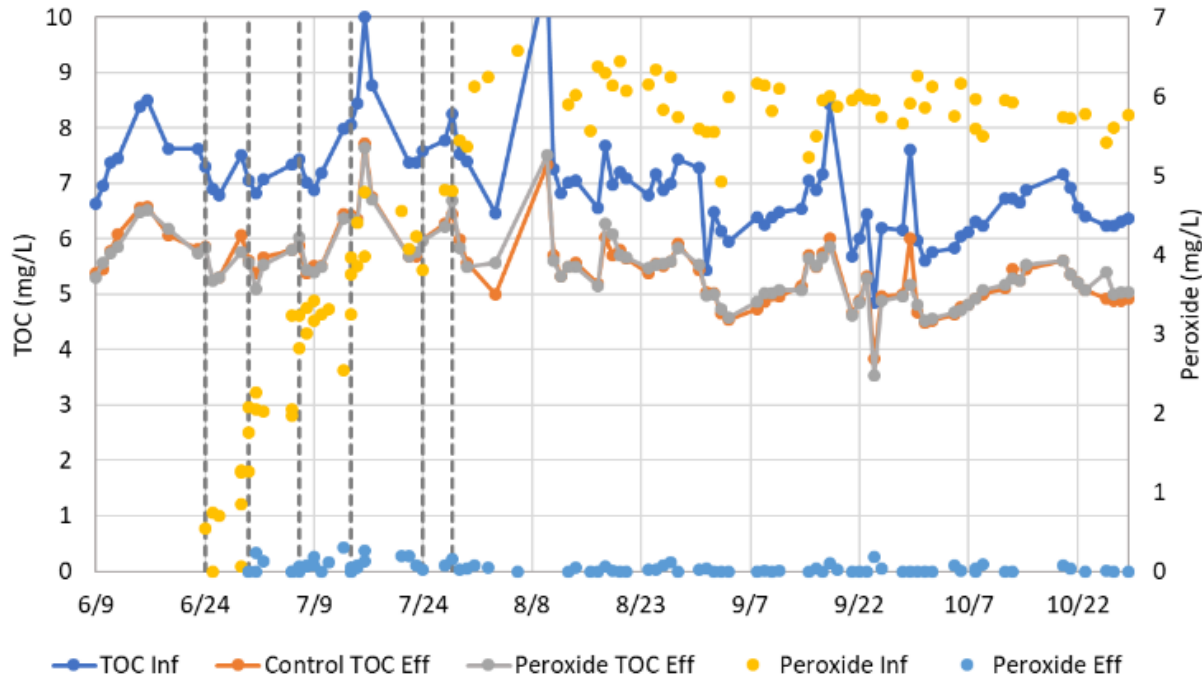
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O₃/H₂O₂ Multi-diffuser Fine Bubble – Pilot Testing

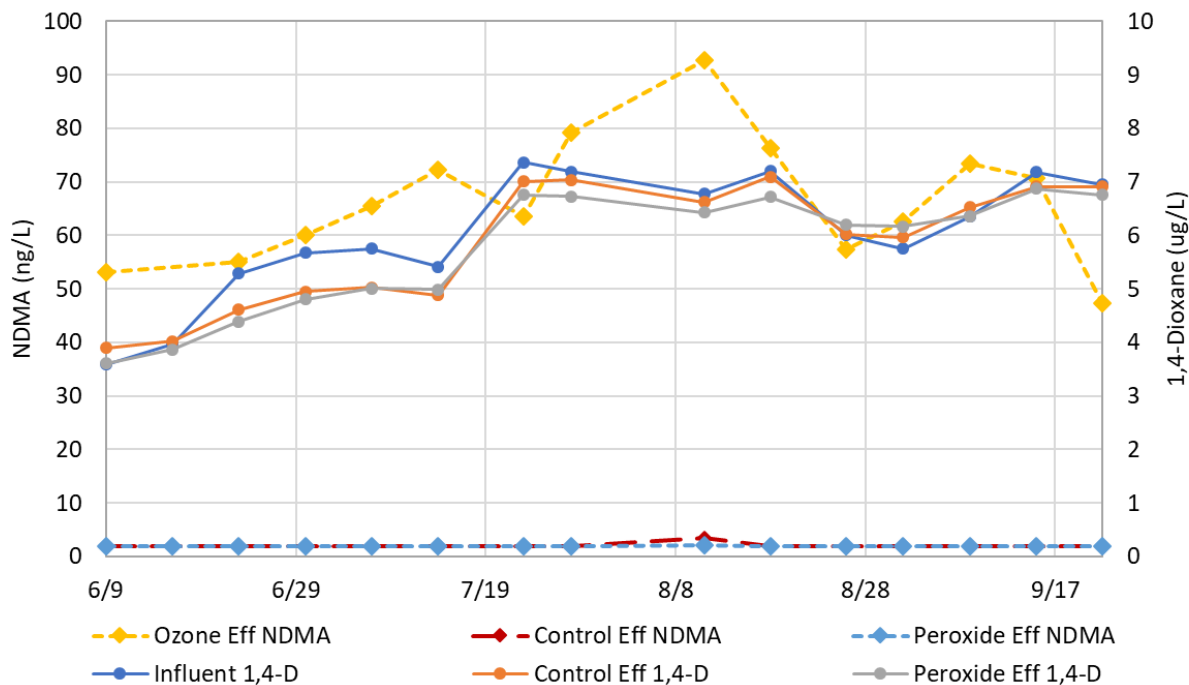


YR DNE Br = 0.398 mg/L

Hydrogen peroxide has no impact on BAF TOC removal



Hydrogen peroxide has no impact on BAF NDMA removal



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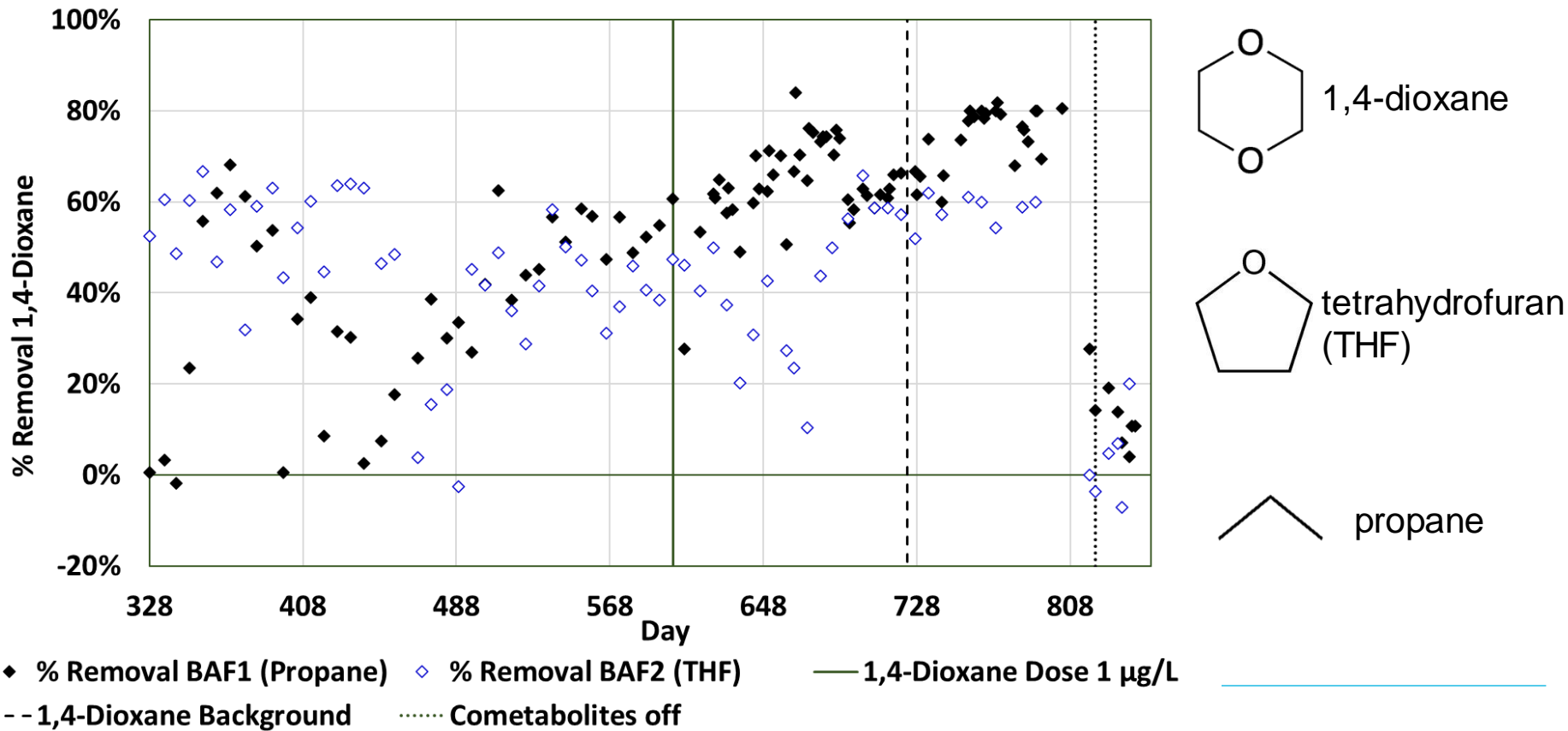
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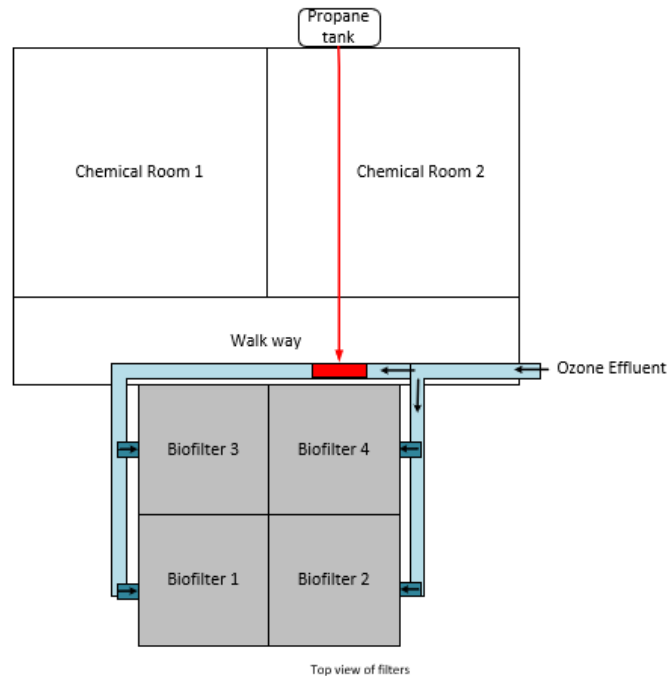
Pilot Propane Feed System



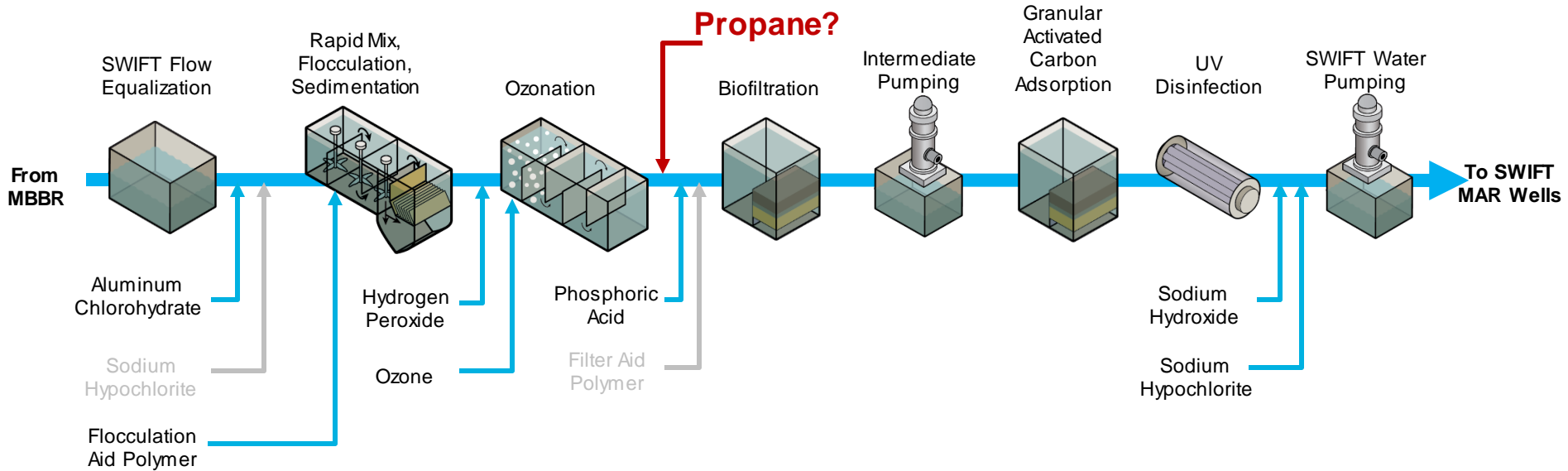
THF and propane have induced similar 1,4-dioxane removal



Full-scale Testing of Propane Feed



James River SWIFT Process Flow Diagram



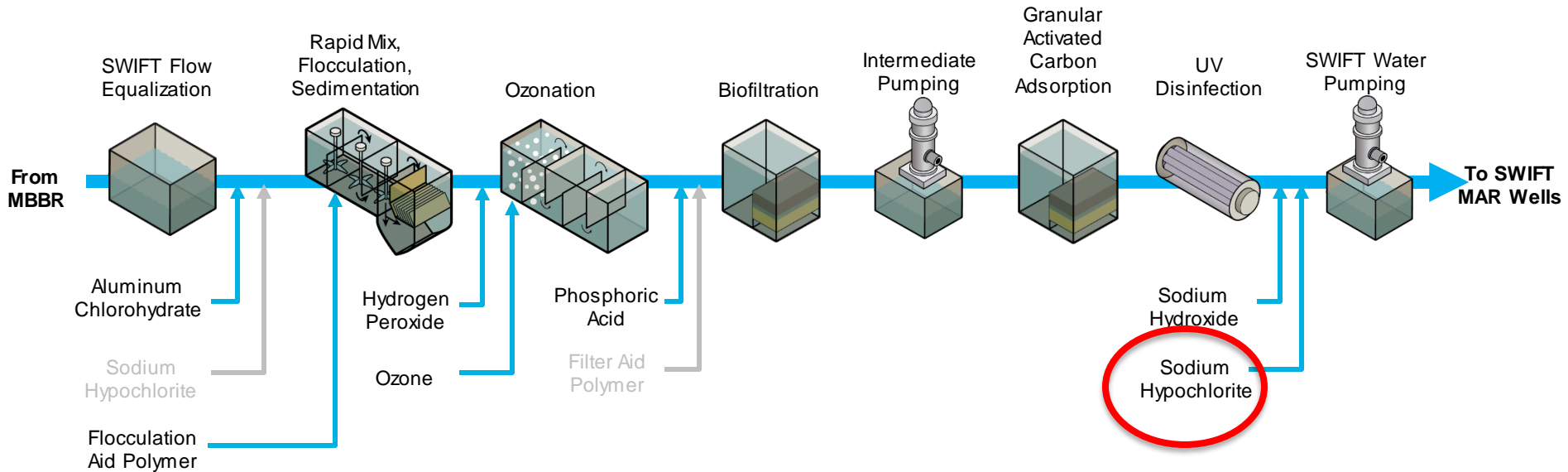
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Ozone + BAF for Wastewater Disinfection?

- as expected, indicator bacteria are very well inactivated by ozone

| | O ₃ :TOC mass/mass | Fecal coliform (MPN/100ml) | Enterococci (MPN/100ml) | Total coliform (MPN/100ml) | <i>E. coli</i> (MPN/100ml) |
|-----------------------------------------------------------------------------------------------|----------------------------------|----------------------------------|----------------------------|----------------------------------|-------------------------------|
| NP secondary clarifier effluent | N/A | 200 | 1450 | 10800 | 98000 |
| Flocculation zone 3 | N/A | 15500 | 399 | 24200 | >24200 |
| Sedimentation effluent | N/A | 135 | <1 | 201 | >2420 |
| Ozone effluent, 1:1 H ₂ O ₂ :O ₃ mass/mass 1 diffuser | 0.2 | 120 | <1 | 201 | >2420 |
| | 0.5 | 2 | <1 | 10 | 172 |
| | 0.8 | <1 | <1 | 4 | 68 |
| Ozone effluent, 1:1 H ₂ O ₂ :O ₃ mass/mass 3 diffusers | 0.2 | 86 | <1 | 129 | 1990 |
| | 0.5 | 2 | 1 | 2 | 34 |
| | 0.8 | 1 | <1 | 3 | 71 |
| Ozone effluent, No chemical addition 3 diffusers | 0.2 | 52 | <1 | 126 | 1550 |
| | 0.5 | 1 | <1 | 1 | 64 |
| | 0.8 | 2 | <1 | 2 | 37 |
| BAF effluent 1 diffuser + H ₂ O ₂ | 0.5 | 1 | <1 | 2 | 11 |
| BAF effluent 3 diffusers + H ₂ O ₂ | 0.5 | <1 | <1 | 4 | 13 |
| BAF effluent 3 diffusers no chem | 0.5 | <1 | <1 | <1 | 11 |

James River VPDES Permit Limits for FIB:

- Fecal Coliform = 200 MPN/100 mL
 - Enterococci = 35 MPN/100 mL
- (monthly average, geometric mean)

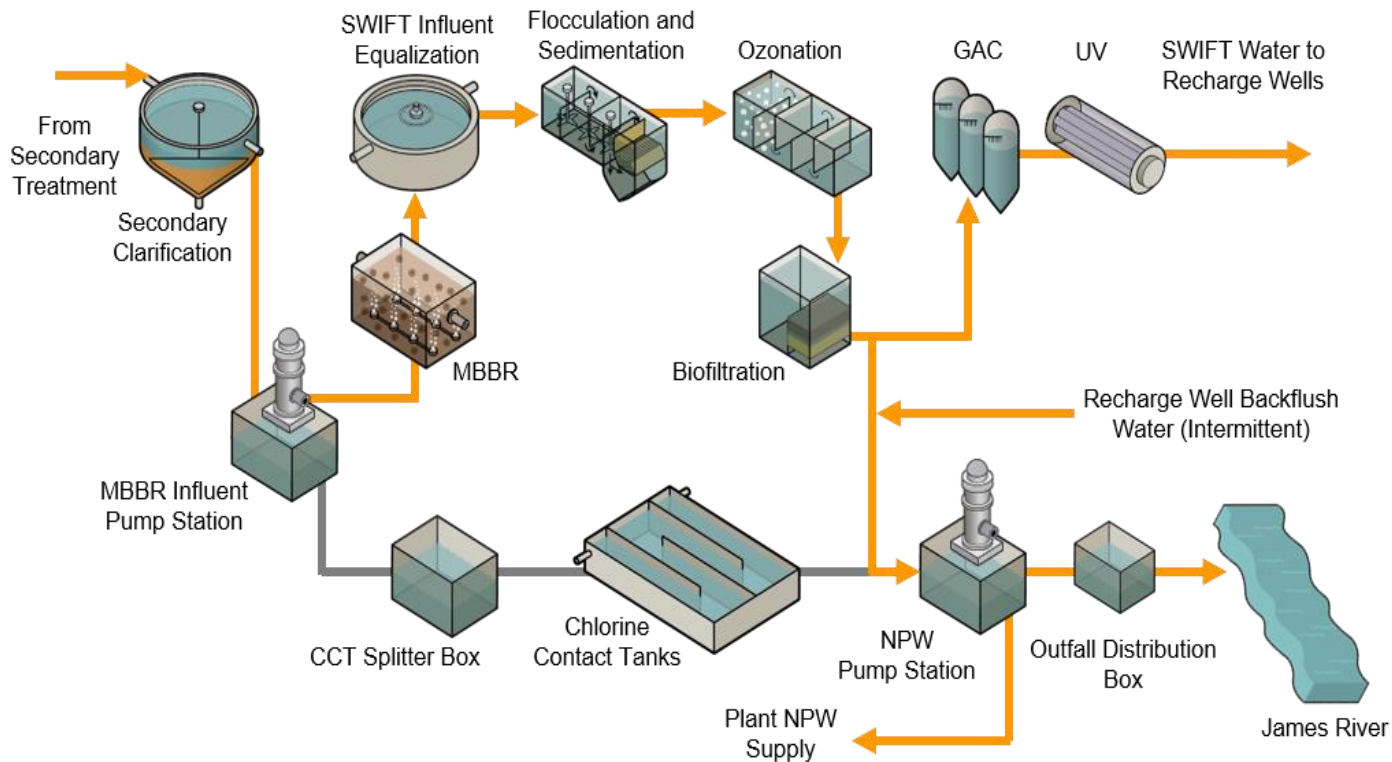
Ozone + BAF for Wastewater Disinfection?

- viral indicators are also inactivated very efficiently

| | O3:TOC mass/mass | Norovirus GI (gc/100ml) | Norovirus GII (gc/100ml) | PMMoV (gc/100ml) |
|-------------------------------------------------------|---------------------|----------------------------|-----------------------------|---------------------|
| NP raw wastewater | | 8.0E2 | 1.73E5 | 9.41E6 |
| NP secondary clarifier effluent | | <16.4 | 3.55E2 | 2.21E5 |
| NP final effluent | | <16.4 | <40.4 | 2.59E5 |
| Settled water | | <1.64 | <4.04 | 1.62E3 |
| Ozone 3 mg/L NH ₂ Cl as Cl ₂ | 0.75 | <1.64 | <4.04 | 9.28E2 |
| Ozone no chemical addition | 0.75 | <1.64 | <4.04 | 1.15E3 |
| Ozone 1:1 H ₂ O ₂ mass/mass | 0.75 | <1.64 | <4.04 | 7.60E1 |
| BAF effluent | | <1.64E-2 | <4.04E-2 | 1.13E-1 |

| | CrAssphage (gc/100ml) | Male specific coliphage (PFU/100ml) | Somatic coliphage (PFU/100ml) |
|-------------------------------------------------------|--------------------------|-------------------------------------------|----------------------------------|
| NP raw wastewater | 5.13E7 | 3.68E4 | 4.73E4 |
| NP secondary clarifier effluent | 2.91E4 | 9.8 | 7.46E2 |
| NP final effluent | 4.45E4 | 6 | 10 |
| Settled water | 29.7 | <0.01 | 2.89 |
| Ozone 3 mg/L NH ₂ Cl as Cl ₂ | 10.7 | <0.01 | <0.01 |
| Ozone no chemical addition | 87.7 | <0.01 | <0.01 |
| Ozone 1:1 H ₂ O ₂ mass/mass | 3.07 | <0.01 | 0.02 |
| BAF effluent | <6.52E-2 | <1E-3 | 1E-3 |

James River - Dry Weather Flow (<16 MGD)



James River - Wet Weather Flow (>16-21 MGD)

